



Water Treatment



Giant Mine Remediation Project



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Outline

- ☐ Underground Water
- ☐ Water Treatment Plant (WTP)
- ☐ Work activities
- ☐ Process & Layout
- ☐ Bench scale tests
- ☐ Sludge Characterization

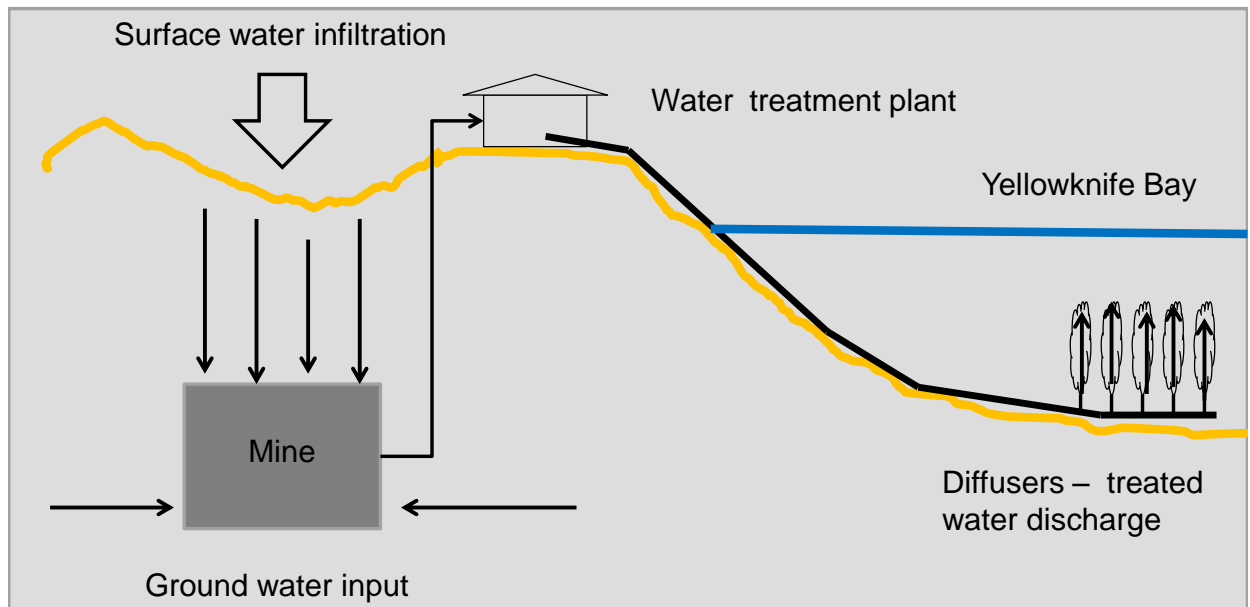
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Overview Mine Water – Collection – Treatment – Discharge



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Yearly Volumes To Be processed (m3)

	Average Year	Wet Year
Pre-Freezing	630,000	822,200
DAR	540,000	
Post Freezing	404,300	517,500
DAR	345,000	

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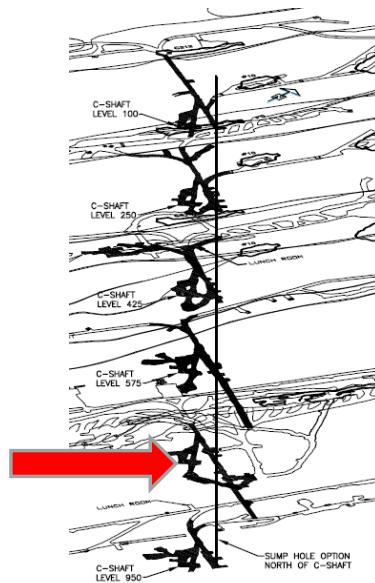


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Initial Raw Water Pump Placement

- 25 m below 750 level near C Shaft
 - Current water level 10 m below 750 at C Shaft



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Design Criteria

Flows & Storage			
Short-Term			
	Average Treatment Flow Rate	26.0	L/s
	Peak Wet Year Flow Rate	33.9	L/s
	Maximum Equalization Storage Volume Required	177,000	m ³
Long-Term			
	Average Treatment Flow Rate	16.7	L/s
	Peak Wet Year Flow Rate	21.3	L/s
	Maximum Equalization Storage Volume Required	0	m ³



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Minewater Quality

- ❑ Parameters of Concern
 - Arsenic
 - Suspended Solids
 - pH
 - Zinc

- ❑ Sampling & Monitoring Program
 - High test (up to 7300 mg As/L)
 - Blended water to surface (est. up to 280 mg As/L)



Performance Criteria

Parameter	Existing Treatment Plant Effluent (2009-2010 data)	New Treatment Plant Effluent (Predicted)	Maximum Average Concentration ^{(a) (b)}	Unit
Ammonia	0.005 – 0.067	No change	12	mg/L
Arsenic (total)	0.205 – 0.418	0.20 target	0.50	mg/L
Total Suspended Solids	<1.0 - 14	<5 (target)	15	mg/L
Nickel	0.0234 – 0.0687	No change	0.50	mg/L
Cyanide	<0.002 – 0.0145	No change	0.80	mg/L
Copper	0.0054 – 0.0162	No change	0.30	mg/L
Lead	<0.0001 - <0.00025	No change	0.20	mg/L
pH	6.24 – 8.96	7.5 – 8.0 (target)	6.5-9.5	units
Radium 226	<0.005 - <1.0	No change	0.37	Bq/L
Zinc	0.0028 – 0.0713	No change	0.20	mg/L
Oil & Grease	0.005 - <2.0	No change	5	mg/L

(a) Based on the former water licence (N1L2-0043) for the existing treatment plant

(b) Maximum rolling average of four consecutive results



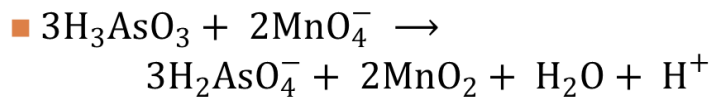
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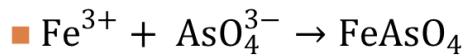
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- Three main steps in arsenic removal

- Oxidation of arsenite to arsenate



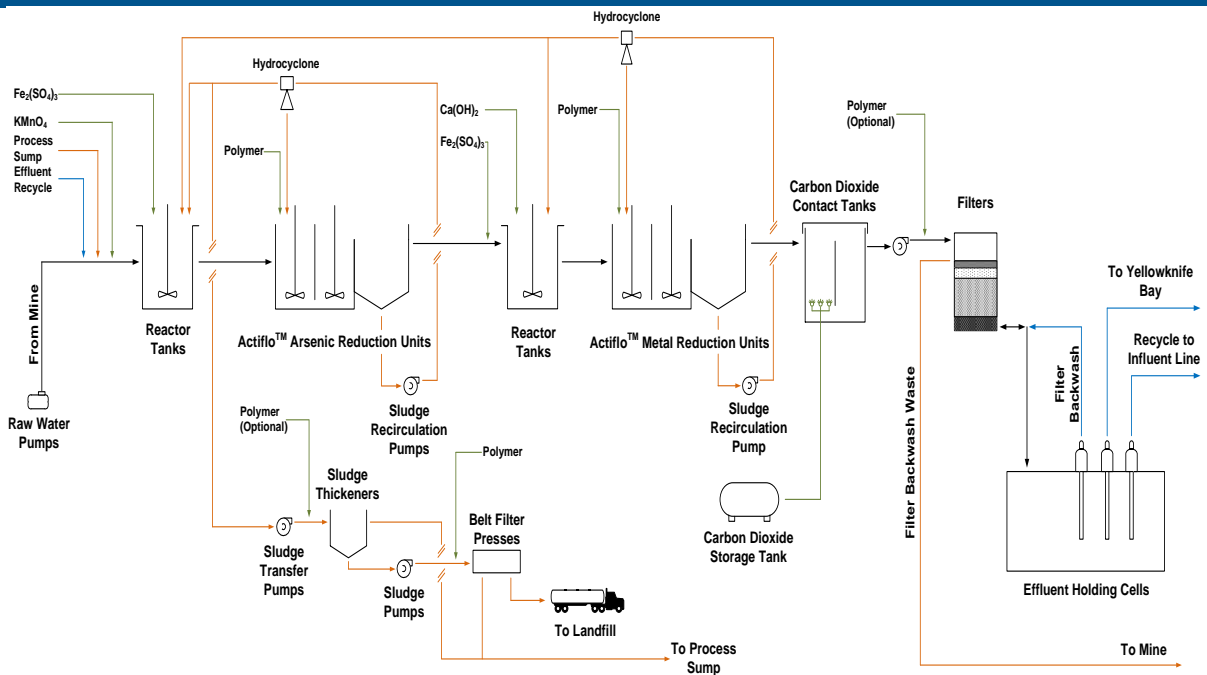
- Precipitation of arsenate



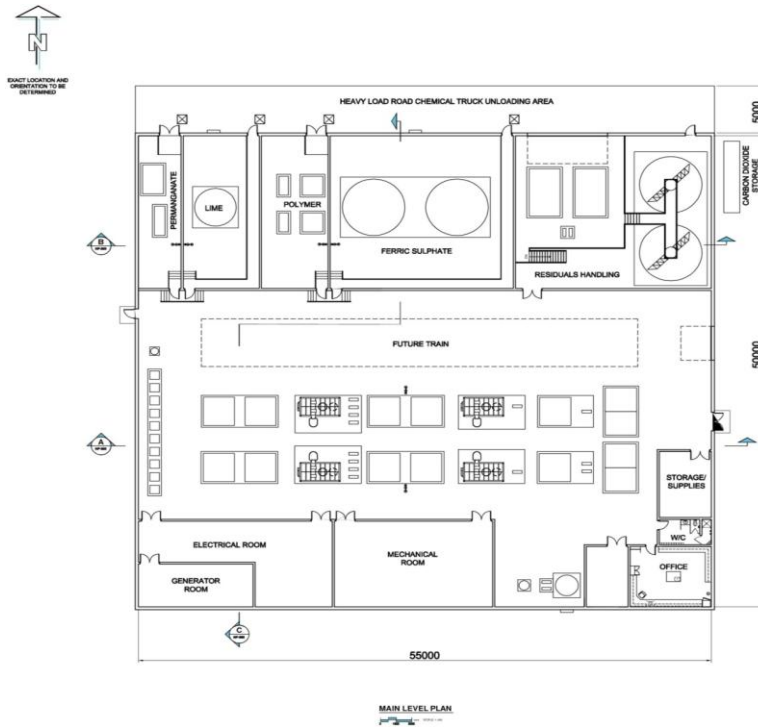
- Removal of precipitate

- Clarification and filtration

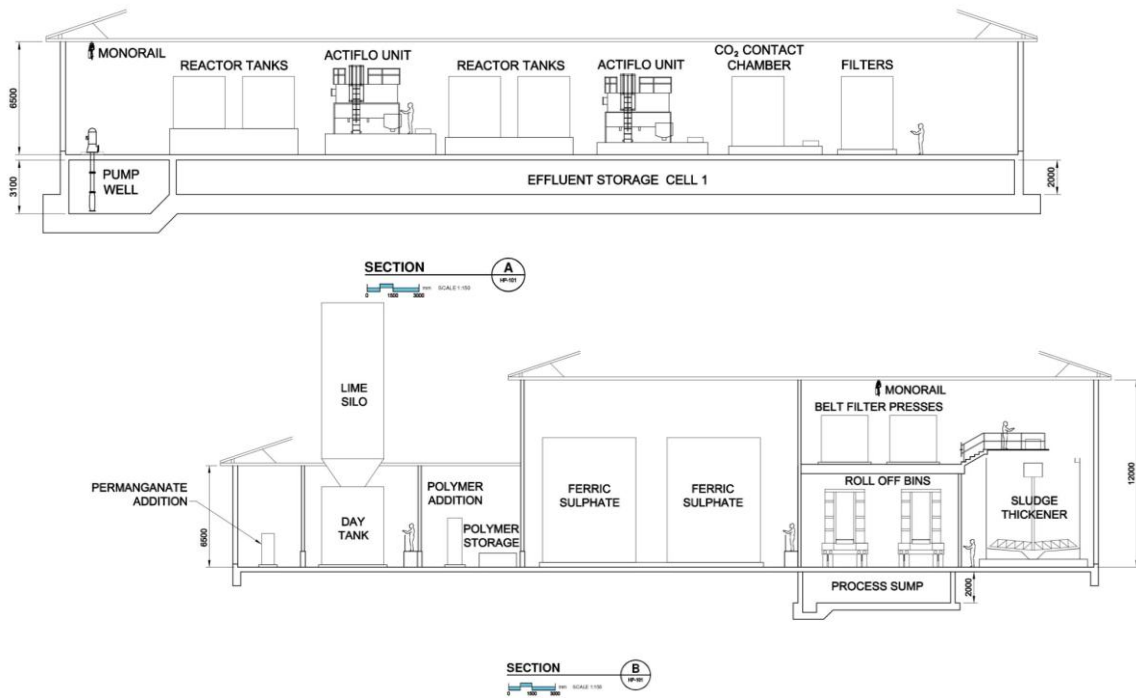
Process Design



Process Design – Process Flow - BAT



Layout -
Plan view



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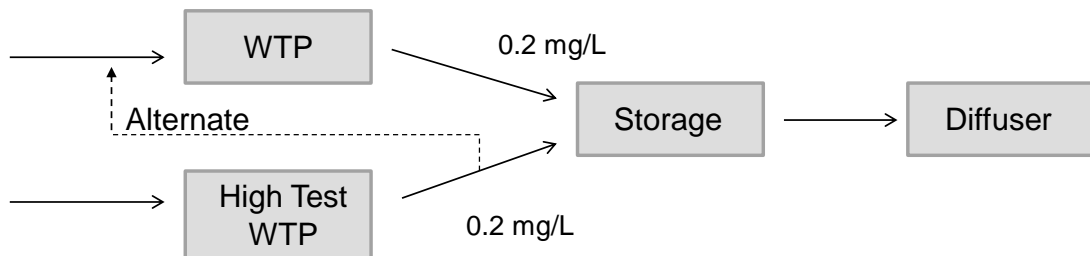


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Potential High Test WTP Component

- ❑ Continued review of a potential separate treatment segment specifically designed to treat high test water.
- ❑ Detail design of WTP is to consider the benefits of:
 - ❑ Retaining the high test piping system & possibly expanding it
 - ❑ A separate treatment segment specifically designed to treat high test water until freeze is completed



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Bench Scale Tests

- ☐ Jar tests are extension of preliminary design activity
- ☐ Jar tests were carried out in Edmonton – March 19 to 23, 2012
- ☐ Objectives
 - ☐ Process Verification
 - ☐ Refine recommended treatment system
 - ☐ Precursor to pilot trials
 - ☐ Confirm chemical choice/process settings
 - ☐ Achieve total Arsenic < 0.1 mg/l
 - ☐ Residuals sampling
 - ☐ Parallel bench scale tests at manufacturers site (April 10 to 24, 2012)



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Main Results

- ❑ Two step process required (i.e. oxidation/coagulation and lime precipitation)
- ❑ Pilot trials identified process achieves total As concentration below 0.2 mg/l
- ❑ Confirmed proposed treatment chemicals
- ❑ Achieved optimized chemical dose rates
- ❑ Lowest chemical dose rates obtained with process alternative (i.e. lime precipitation followed by oxidation/coagulation)
- ❑ Confirmed treatment process for next level of design



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Sludge Characterization

- ☐ samples of the sludge generated from the ETP and deposited in the settling pond were sampled on March 12, 2012
- ☐ Composite sample collected using a backhoe reaching into the sediments at the base of the settling pond
- ☐ Leachable arsenic analysis performed

	ETP Sludge	
Sample Number	Total Arsenic Detection Limit of 0.10 mg/kg	Leachable Arsenic (TCLP) Detection Limit of 0.20 mg/L
S.P. 1	17,400 mg/kg	0.23 mg/L
S.P. 2	22,700 mg/kg	<0.20 mg/L

- ☐ Sludge not classified as a hazardous waste

